

## Radiation And Dissipation On The Convective Heat Transfer Flow Of A Viscous Fluid Through A Porous Medium In A Rectangular Cavity Using Darcy Model

**C. Sulochana, Sharanamma V Aounti**  
Gulbarga University Gulbarga,  
Govt. First Grade College Jewargi, Gulbarga

### ABSTRACT:

In this chapter an attempt has been made to discuss the combined influence of radiation and dissipation on the convective heat transfer flow of a viscous fluid through a porous medium in a rectangular cavity using Darcy model. Making use of the incompressibility the governing non-linear coupled equations for the momentum, energy and diffusion are derived in terms of the non-dimensional stream function, temperature. The Galerkin finite element analysis with linear triangular elements is used to obtain the Global stiffness matrices for the values of stream function, temperature. These coupled matrices are solved using iterative procedure and expressions for the stream function, temperature are obtained as linear combinations of the shape functions. The behavior of temperature and Nusselt number are discussed computationally for different values of the governing Parameters  $Ra$ ,  $\alpha$ ,  $N_1$  and  $Ec$ .

**Keywords:** Heat Transfer, Porous Medium, Rectangular duct, Finite Element Analysis

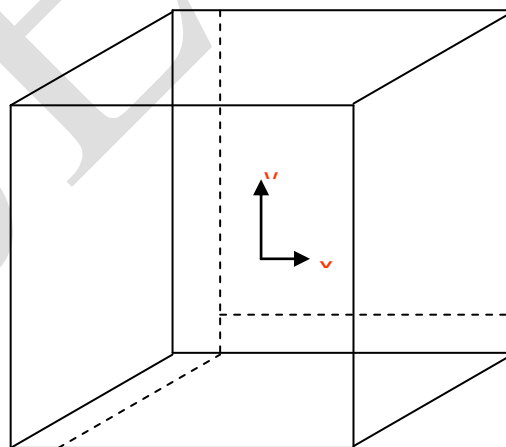


Fig. i

### SCHEMATIC DIAGRAM OF THE FLOW MODEL

## **FORMULATION OF THE PROBLEM**

We consider the mixed convective heat transfer flow of a viscous incompressible fluid in a saturated porous medium confined in the rectangular duct (Fig. 1) whose base length is  $a$  and height  $b$ . The heat flux on the base and top walls is maintained constant. The Cartesian coordinate system  $O(x, y)$  is chosen with origin on the central axis of the duct and its base parallel to  $x$ -axis.

We assume that

- i) The convective fluid and the porous medium are everywhere in local thermodynamic equilibrium.
- ii) There is no phase change of the fluid in the medium.
- iii) The properties of the fluid and of the porous medium are homogeneous and isotropic.
- iv) The porous medium is assumed to be closely packed so that Darcy's momentum law is adequate in the porous medium.
- v) The Boussinesq approximation is applicable.

Under these assumption the governing equations are given by

$$\frac{\partial u'}{\partial x'} + \frac{\partial v'}{\partial y'} = 0 \quad (2.1)$$

$$u' = -\frac{k}{\mu} \left( \frac{\partial p'}{\partial x'} \right) \quad (2.2)$$

$$v' = -\frac{k}{\mu} \left( \frac{\partial p'}{\partial y'} + \rho' g \right) \quad (2.3)$$

$$\rho_{\sigma} c_p \left( u' \frac{\partial T'}{\partial x'} + v' \frac{\partial T'}{\partial y'} \right) = K_1 \left( \frac{\partial^2 T'}{\partial x'^2} + \frac{\partial^2 T'}{\partial y'^2} \right) + Q(T_0 - T) + \left( \frac{\mu}{K} \right) (u'^2 + v'^2) - \frac{\partial(q_r)}{\partial x} \quad (2.4)$$

$$\rho' = \rho_0 \{ 1 - \beta(T' - T_0) \} \quad (2.5)$$

$$T_0 = \frac{T_h + T_c}{2},$$

Where  $u'$  and  $v'$  are Darcy velocities along direction of  $\theta(x, y)$ ,  $T'$ ,  $p'$  and  $g'$  are the temperature, pressure and acceleration due to gravity,  $T_c$ , and  $T_h$  are the temperature on the

cold and warm side walls respectively.  $\rho'$ ,  $\mu$ ,  $\nu$ , and  $\beta$  are the density, coefficients of viscosity, kinematic viscosity and thermal expansion of the fluid,  $k$  is the permeability of the porous medium,  $K_1$  is the thermal conductivity,  $C_p$  is the specific heat at constant pressure,  $Q$  is the strength of the heat source,  $k_{11}$  is the cross diffusivity,  $\mu_e$  is the magnetic permeability of the medium and  $q_r$  is the radiative heat flux.

The boundary conditions are

$$\begin{aligned} u' = v' = 0 & \quad \text{on the boundary of the duct} \\ T' = T_c, & \quad \text{on the side wall to the left} \\ T' = T_h, & \quad \text{on the side wall to the right} \\ \frac{\partial T'}{\partial y} = 0, & \quad \text{on the top (y = 0) and bottom} \\ u = v = 0 & \quad \text{walls (y = 0) which are insulated.} \end{aligned} \tag{2.6}$$

Invoking Rosseland approximation for radiation

$$q_r = \frac{4\sigma^*}{3\beta_R} \frac{\partial T'^4}{\partial y}$$

Expanding  $T'^4$  in Taylor's series about  $T_e$  and neglecting higher order terms

$$T'^4 \cong 4T_e^3 T' - 3T_e^4$$

We now introduce the following non-dimensional variables

$$\begin{aligned} x' = ax; \quad y' = by; \quad c = b/a; \quad u' = (v/a)u; \\ v' = (v/a)v; \quad p' = (v^2 \rho/a^2)p; \quad T' = T_0 + \theta (T_h - T_c) \end{aligned} \tag{2.7}$$

The governing equations in the non-dimensional form are

$$u = -\left(\frac{K}{a^2}\right) \frac{\partial p}{\partial x} \tag{2.8}$$

$$v = -\frac{k}{a^2} \frac{\partial p}{\partial y} - \frac{kag}{v^2} + \frac{kag\beta(T_h - T_c)\theta}{v^2} - \left(\frac{\sigma\mu_e^2 H_0^2 k}{\mu}\right)v \tag{2.9}$$

$$P\left(u \frac{\partial \theta}{\partial x} + v \frac{\partial \theta}{\partial y}\right) = \left(1 + \frac{4N}{3}\right) \left(\frac{\partial^2 \theta}{\partial x^2} + \frac{\partial^2 \theta}{\partial y^2}\right) - \alpha\theta + E_C(u^2 + v^2) \tag{2.10}$$

In view of the equation of continuity we introduce the stream function  $\psi$  as

$$u = \frac{\partial \psi}{\partial y}; \quad v = -\frac{\partial \psi}{\partial x} \tag{2.11}$$

Eliminating  $p$  from the equation (2.8) and (2.9) and making use of (2.10) the equations in terms of  $\psi$  and  $\theta$  are

$$\nabla^2 \psi = -Ra \left( \frac{\partial \theta}{\partial x} \right) \quad (2.12)$$

$$P \left( \frac{\partial \psi}{\partial y} \frac{\partial \theta}{\partial x} - \frac{\partial \psi}{\partial x} \frac{\partial \theta}{\partial y} \right) = \left( 1 + \frac{4}{3N_1} \right) \left( \frac{\partial^2 \theta}{\partial x^2} + \frac{\partial^2 \theta}{\partial y^2} \right) - \alpha \theta + Ec \left( \left( \frac{\partial \psi}{\partial y} \right)^2 + \left( \frac{\partial \psi}{\partial x} \right)^2 \right) \quad (2.13)$$

Where

$$G = \frac{g\beta(T_h - T_c)a^3}{\nu^2} \quad (\text{Grashoff number})$$

$$D^{-1} = \frac{a^2}{k} \quad (\text{Darcy parameter})$$

$$P = \mu c_p / K_1 \quad (\text{Prandtl number})$$

$$\alpha = Qa^2 / K_1 \quad (\text{Heat source parameter})$$

$$Ra = \frac{\beta g (T_g - T_c) k a}{\nu^2} \quad (\text{Rayleigh Number})$$

$$N_1 = \frac{3\beta_R K_1}{4\sigma \cdot T_e^3} \quad (\text{Radiation parameter})$$

$$Ec = \left( \frac{a^4}{\mu K K_1 \Delta T} \right) \quad (\text{Eckert number})$$

The boundary conditions are

$$\frac{\partial \psi}{\partial x} = 0, \frac{\partial \psi}{\partial y} = 0 \text{ on } x = 0 \text{ \& \;} 1 \quad (2.14)$$

$$\theta = 1 \text{ on } x = 0$$

$$\theta = 0 \text{ on } x = 1 \quad (2.15)$$

## **FINITE ELEMENT ANALYSIS and SOLUTION OF THE PROBLEM**

The region is divided into a finite number of three node triangular elements, in each of which the element equation is derived using Galerkin weighted residual method. In each element  $f_i$  the approximate solution for an unknown  $f$  in the variational formulation is expressed as a linear combination of shape function.  $(N_k^i)_{k=1,2,3}$ , which are linear polynomials in  $x$  and  $y$ . This approximate solution of the unknown  $f$  coincides with actual values at each node of the element. The variational formulation results in a  $3 \times 3$  matrix equation (stiffness matrix) for the unknown local nodal values of the given element. These stiffness matrices are assembled in terms of global nodal values using inter element continuity and boundary conditions resulting in global matrix equation.

In each case there are  $r$  distinct global nodes in the finite element domain and  $f_p$  ( $p = 1, 2, \dots, r$ ) is the global nodal values of any unknown  $f$  defined over the domain then

$$f = \sum_{i=1}^8 \sum_{p=1}^r f_p \Phi_p^i,$$

where the first summation denotes summation over  $s$  elements and the second one represents summation over the independent global nodes and

$$\begin{aligned} \Phi_p^i &= N_N^i, \text{ if } p \text{ is one of the local nodes say } k \text{ of the element } e_i \\ &= 0, \text{ otherwise.} \end{aligned}$$

$f_p$ 's are determined from the global matrix equation. Based on these lines we now make a finite element analysis of the given problem governed by (2.12) - (2.13) subjected to the conditions (2.14) - (2.15).

Let  $\psi^i$  and  $\theta^i$  be the approximate values of  $\psi$  and  $\theta$  in an element  $\theta_i$ .

$$\psi^i = N_1^i \psi_1^i + N_2^i \psi_2^i + N_3^i \psi_3^i \quad (3.1a)$$

$$\theta^i = N_1^i \theta_1^i + N_2^i \theta_2^i + N_3^i \theta_3^i \quad (3.1b)$$

Substituting the approximate value  $\psi^i$  and  $\theta^i$  for  $\psi$  and  $\theta$  respectively in (2.13), the error

$$E_1^i = \left(1 + \frac{4}{3N_1}\right) \frac{\partial^2 \theta^i}{\partial x^2} + \frac{\partial^2 \theta^i}{\partial y^2} - P \left( \frac{\partial \psi^i}{\partial y} \frac{\partial \theta^i}{\partial x} - \frac{\partial \psi^i}{\partial x} \frac{\partial \theta^i}{\partial y} \right) - \alpha \theta + E_c \left[ \left( \frac{\partial \psi}{\partial y} \right)^2 + \left( \frac{\partial \psi}{\partial x} \right)^2 \right] \quad (3.2)$$

Under Galerkin method this error is made orthogonal over the domain of  $e_i$  to the respective shape functions (weight functions) where

$$\int_{e_i} E_1^i N_k^i d\Omega = 0,$$

$$\int_{e_i} E_2^i N_k^i d\Omega = 0$$

$$\int_{e_i} N_k^i \left[ \left(1 + \frac{4}{3N_1}\right) \left( \frac{\partial^z \theta^i}{\partial x^2} + \frac{\partial^z \theta^i}{\partial y^2} \right) - P \left( \frac{\partial \psi^i}{\partial y} \frac{\partial \theta^i}{\partial x} - \frac{\partial \psi^i}{\partial x} \frac{\partial \theta^i}{\partial y} \right) - \alpha \theta + \left[ E_c \left( \frac{\partial \psi}{\partial y} \right)^2 + \left( \frac{\partial \psi}{\partial x} \right)^2 \right] \right] d\Omega = 0 \quad (3.4)$$

Using Green's theorem we reduce the surface integral (3.4)&(3.5) without affecting  $\psi$  terms and obtain

$$\int_{e_i} N_k^i \left\{ \left(1 + \frac{4}{3N_1}\right) \frac{\partial N_k^i}{\partial x} \frac{\partial \theta^i}{\partial x} + \frac{\partial N_k^i}{\partial y} \frac{\partial \theta^i}{\partial y} - P N_k^i \left( \frac{\partial \psi^i}{\partial y} \frac{\partial \theta^i}{\partial x} - \frac{\partial \psi^i}{\partial x} \frac{\partial \theta^i}{\partial y} \right) - \alpha \theta + E_c \left[ \left( \frac{\partial \psi}{\partial y} \right)^2 + \left( \frac{\partial \psi}{\partial x} \right)^2 \right] \right\} d\Omega$$

$$= \int_{\Gamma_i} N_k^i \left( \frac{\partial \theta^i}{\partial x} n_x + \frac{\partial \theta^i}{\partial y} n_y \right) d\Gamma_i \quad (3.6)$$

where  $\Gamma_i$  is the boundary of  $e_i$ .

Substituting L.H.S. of (3.1a)- (3.1b) for  $\psi^i$  and  $\theta^i$  in (3.6) we get

$$\sum_1 \int_{e_i} \left(1 + \frac{4N}{3}\right) \frac{\partial N_k^i}{\partial x} \frac{\partial N_L^i}{\partial x} + \frac{\partial N_L^i}{\partial y} \frac{\partial N_k^i}{\partial y} - P \sum_1 \psi_m^i \int_{e_i} \left( \frac{\partial N_m^i}{\partial y} \frac{\partial N_L^i}{\partial x} - \frac{\partial N_m^i}{\partial x} \frac{\partial N_L^i}{\partial y} \right) d\Omega$$

$$- \alpha \sum_{e_i} \theta^i \int N N_k^i d\Omega + E_c \int_{e_i} \left[ \left( \frac{\partial \psi}{\partial y} \right)^2 + \left( \frac{\partial \psi}{\partial x} \right)^2 \right] d\Omega$$

$$= \int_{\Gamma_i} N_k^i \left( \frac{\partial \theta^i}{\partial x} n_x + \frac{\partial \theta^i}{\partial y} n_y \right) d\Gamma_i = Q_k^i \quad (l, m, k = 1,2,3) \quad (3.8)$$

where

$Q_k^i = Q_{k1}^i + Q_{k2}^i + Q_{k3}^i$ ,  $Q_k^i$ 's being the values of  $Q_k^i$  on the sides  $s = (1,2,3)$  of the element  $e_i$ . The sign of  $Q_k^i$ 's depends on the direction of the outward normal w.r.t the element.

Choosing different  $N_k^i$ 's as weight functions and following the same procedure we obtain matrix equations for three unknowns ( $Q_p^i$ ) viz.,

$$(a_p^i)(\theta_p^i) = (Q_k^i) \quad (3.10)$$

where  $(a_{pk}^i)$  is a 3 x 3 matrix,  $(\theta_p^i), (Q_k^i)$  are column matrices.

Repeating the above process with each of  $s$  elements, we obtain sets of such matrix equations. Introducing the global coordinates and global values for  $\theta_p^i$  and making use of inter element continuity and boundary conditions relevant to the problem the above stiffness matrices are assembled to obtain a global matrix equation. This global matrix is  $r \times r$  square matrix if there are  $r$  distinct global nodes in the domain of flow considered.

Similarly substituting  $\psi^i$  and  $\theta^i$  in (2.12) and defining the error

$$E_3^i = \nabla^2 \psi + Ra \left( \frac{\partial \theta}{\partial x} + N \frac{\partial \phi}{\partial x} \right) \quad (3.11)$$

and following the Galerkin method we obtain

$$\int_{\Omega} E_3^i \psi_j^i d\Omega = 0 \quad (3.12)$$

Using Green's theorem (3.8) reduces to

$$\begin{aligned} & \int_{\Omega} \left( \frac{\partial N_k^i}{\partial x} \frac{\partial \psi^i}{\partial x} + \frac{\partial N_k^i}{\partial y} \frac{\partial \psi^i}{\partial y} + Ra \left( \theta^i \frac{\partial N_k^i}{\partial x} \right) \right) d\Omega \\ &= \int_{\Gamma} N_k^i \left( \frac{\partial \psi^i}{\partial x} n_x + \frac{\partial \psi^i}{\partial y} n_y \right) d\Gamma_i + \int_{\Gamma} N_k^i n_x \theta^i d\Gamma_i \end{aligned} \quad (3.13)$$

In obtaining (3.13) the Green's theorem is applied w.r.t derivatives of  $\psi$  without affecting  $\theta$  terms.

Using (3.1) and (3.2) in (3.13) we have

$$\sum_m \psi_m^i \left\{ \int_{\Omega} \left( \frac{\partial N_k^i}{\partial x} \frac{\partial N_m^i}{\partial x} + \frac{\partial N_m^i}{\partial y} \frac{\partial N_k^i}{\partial y} \right) d\Omega + Ra \sum_L (\theta_L^i \int_{\Omega} N_k^i \frac{\partial N_L^i}{\partial x} d\Omega) \right\}$$

$$= \int_{\Gamma} N_k^i \left( \frac{\partial \psi^i}{\partial x} n_x + \frac{\partial \psi^i}{\partial y} n_y \right) d\Gamma_i + \int_{\Gamma} N_k^i \theta^i d\Omega_i = \Gamma_k^i \quad (3.14)$$

In the problem under consideration, for computational purpose, we choose uniform mesh of 10 triangular elements. The domain has vertices whose global coordinates are (0,0), (1,0) and (1,c) in the non-dimensional form. Let  $e_1, e_2, \dots, e_{10}$  be the ten elements and let  $\theta_1, \theta_2, \dots, \theta_{10}$  be the global values of  $\theta$  and  $\psi_1, \psi_2, \dots, \psi_{10}$  be the global values of  $\psi$  at the ten global nodes of the domain

### **SHAPE FUNCTIONS and STIFFNESS MATRICES**

Range functions in  $n_{i,j}$ ;  $i = \text{element}, j = \text{node}$ .

$n_{1,1} = 1 - 3x$	$n_{1,2} = 3x - \frac{3y}{C}$	$n_{2,1} = 1 - \frac{3y}{C}$	$n_{2,2} = -1 + \frac{3y}{C}$
$n_{2,3} = 1 - 3x + \frac{3y}{C}$	$n_{3,1} = 2 - 3x$	$n_{3,2} = -1 + 3x - \frac{3y}{C}$	$n_{3,3} = \frac{3y}{C}$
$n_{4,1} = 1 - \frac{3y}{C}$	$n_{4,2} = -2 + 3x$	$n_{4,3} = 2 - 3x + \frac{3y}{C}$	$n_{5,1} = 2 - 3x$
$n_{5,2} = -1 + 3x - \frac{3y}{C}$	$n_{5,3} = \frac{3y}{C}$	$n_{6,1} = 2 - 3x$	$n_{6,2} = 3x - \frac{3y}{C}$
$n_{6,3} = 1 + \frac{3y}{C}$	$n_{7,1} = 2 - \frac{3y}{C}$	$n_{7,2} = -2 + 3x$	$n_{7,3} = 1 - 3x + \frac{3y}{C}$
$n_{8,1} = 3 - 3x$	$n_{8,2} = -1 + 3x - \frac{3y}{C}$	$n_{9,2} = 3x - \frac{3y}{C}$	$n_{9,3} = -1 + \frac{3y}{C}$

Substituting the vabove shape functions in (3.8),(3.9)&(3.14) w.r.t each element and integrating over the respective triangular domain we obtain the element in the form (3.8).The 3x3 matrix equations are assembled using connectivity conditions to obtain a 8x8 matrix equations for the global nodes  $\psi_p, \theta_p$  and  $\phi_p$ .

The global matrix equation for  $\theta$  is

$$A_3 X_3 = B_3 \quad (4.1)$$

The global matrix equation for  $\psi$  is

$$A_5 X_5 = B_5 \quad (4.3)$$



The global matrix equations are coupled and are solved under the following iterative procedures. At the beginning of the first iteration the values of  $(\psi_i)$  are taken to be zero and the global equations (4.1)&(4.2) are solved for the nodal values of  $\theta$  and  $\phi$ . These nodal values  $(\theta_i)$  and  $(\phi_i)$  obtained are then used to solve the global equation (4.3) to obtain  $(\psi_i)$ . In the second iteration these  $(\psi_i)$  values are obtained are used in (4.1)&(4.2) to calculate  $(\theta_i)$  and  $(\phi_i)$  and vice versa. The three equations are thus solved under iteration process until two consecutive iterations differ by a pre-assigned percentage.

The domain consists three horizontal levels and the solution for  $\Psi$  &  $\theta$  at each level may be expressed in terms of the nodal values as follows,

In the horizontal strip  $0 \leq y \leq \frac{c}{3}$

$$\begin{aligned} \Psi &= (\Psi_1 N^1_1 + \Psi_2 N^1_2 + \Psi_7 N^1_7) H(1 - \tau_1) \\ &= \Psi_1 (1 - 4x) + \Psi_2 4(x - \frac{y}{c}) + \Psi_7 (\frac{4y}{c} (1 - \tau_1)) \end{aligned} \quad (0 \leq x \leq \frac{1}{3})$$

$$\begin{aligned} \Psi &= (\Psi_2 N^3_2 + \Psi_3 N^3_3 + \Psi_6 N^3_6) H(1 - \tau_2) \\ &+ (\Psi_2 N^2_2 + \Psi_7 N^2_7 + \Psi_6 N^2_6) H(1 - \tau_3) \end{aligned} \quad (\frac{1}{3} \leq x \leq \frac{1}{3})$$

$$\begin{aligned} &= (\Psi_2 2(1 - 2x) + \Psi_3 (4x - \frac{4y}{c} - 1) + \Psi_6 (\frac{4y}{c})) H(1 - \tau_2) \\ &+ (\Psi_2 (1 - \frac{4y}{c}) + \Psi_7 (1 + \frac{4y}{c} - 4x) + \Psi_6 (4x - 1)) H(1 - \tau_3) \end{aligned}$$

$$\begin{aligned} \Psi &= (\Psi_3 N^5_3 + \Psi_4 N^5_4 + \Psi_5 N^5_5) H(1 - \tau_3) \\ &+ (\Psi_3 N^4_3 + \Psi_5 N^4_5 + \Psi_6 N^4_6) H(1 - \tau_4) \end{aligned} \quad (\frac{2}{3} \leq x \leq 1)$$

$$\begin{aligned} &= (\Psi_3 (3 - 4x) + \Psi_4 2(2x - \frac{2y}{c} - 1) + \Psi_6 (\frac{4y}{c} - 4x + 3)) H(1 - \tau_3) \\ &+ \Psi_3 (1 - \frac{4y}{c}) + \Psi_5 (4x - 3) + \Psi_6 (\frac{4y}{c}) H(1 - \tau_4) \end{aligned}$$

Along the strip  $\frac{c}{3} \leq y \leq \frac{2c}{3}$

$$\Psi = (\Psi_7 N^6_7 + \Psi_6 N^6_6 + \Psi_8 N^6_8) H(1 - \tau_2) \quad (\frac{1}{3} \leq x \leq 1)$$

$$+ (\Psi_6 N^7_6 + \Psi_9 N^7_9 + \Psi_8 N^7_8) H(1 - \tau_3) + (\Psi_6 N^8_6 + \Psi_5 N^8_5 + \Psi_9 N^8_9) H(1 - \tau_4)$$

$$\Psi = (\Psi_7 2(1-2x) + \Psi_6 (4x-3) + \Psi_8 (\frac{4y}{c} - 1))H(1 - \tau_3)$$

$$+ \Psi_6 (2(1 - \frac{2y}{c}) + \Psi_9 (\frac{4y}{c} - 1) + \Psi_8 (1 + \frac{4y}{c} - 4x))H(1 - \tau_4)$$

$$+ \Psi_6 (4(1-x) + \Psi_5 (4x - \frac{4y}{c} - 1) + \Psi_9 2(\frac{2y}{c} - 1))H(1 - \tau_5)$$

Along the strip  $\frac{2c}{3} \leq y \leq 1$

$$\Psi = (\Psi_8 N^9_8 + \Psi_9 N^9_9 + \Psi_{10} N^9_{10}) H(1 - \tau_6) \quad (\frac{2}{3} \leq x \leq 1)$$

$$= \Psi_8 (4(1-x) + \Psi_9 4(x - \frac{y}{c}) + \Psi_{10} 2(\frac{4y}{c} - 3))H(1 - \tau_6)$$

where  $\tau_1 = 4x$ ,  $\tau_2 = 2x$ ,  $\tau_3 = \frac{4x}{3}$ ,

$$\tau_4 = 4(x - \frac{y}{c}), \quad \tau_5 = 2(x - \frac{y}{c}), \quad \tau_6 = \frac{4}{3}(x - \frac{y}{c})$$

and H represents the Heaviside function.

The expressions for  $\theta$  are

In the horizontal strip  $0 \leq y \leq \frac{c}{3}$

$$\theta = [\theta_1(1-4x) + \theta_2 4(x - \frac{y}{c}) + \theta_7 (\frac{4y}{c})] H(1 - \tau_1) \quad (0 \leq x \leq \frac{1}{3})$$

$$\theta = (\theta_2(2(1-2x) + \theta_3 (4x - \frac{4y}{c} - 1) + \theta_6 (\frac{4y}{c})) H(1 - \tau_2)$$

$$+ \theta_2(1 - \frac{4y}{c}) + \theta_7(1 + \frac{4y}{c} - 4x) + \theta_6(4x - 1))H(1 - \tau_3) \quad (\frac{1}{3} \leq x \leq \frac{2}{3})$$

$$\theta = \theta_3(3-4x) + 2\theta_4(2x - \frac{2y}{c} - 1) + \theta_6(\frac{4y}{c} - 4x + 3) H(1 - \tau_3)$$

$$+ (\theta_3(1 - \frac{4y}{c}) + \theta_5(4x - 3) + \theta_6(\frac{4y}{c})) H(1 - \tau_4) \quad (\frac{2}{3} \leq x \leq 1)$$

Along the strip  $\frac{c}{3} \leq y \leq \frac{2c}{3}$

$$\theta = (\theta_7(2(1-2x)) + \theta_6(4x-3) + \theta_8(\frac{4y}{c}-1)) H(1-\tau_3) \quad (\frac{1}{3} \leq x \leq \frac{2}{3})$$

$$+(\theta_6(2(1-\frac{2y}{c})) + \theta_9(\frac{4y}{c}-1) + \theta_8(1+\frac{4y}{c}-4x)) H(1-\tau_4)$$

$$+(\theta_6(4(1-x)) + \theta_5(4x-\frac{4y}{c}-1) + \theta_9(2(\frac{4y}{c}-1))) H(1-\tau_5)$$

Along the strip  $\frac{2c}{3} \leq y \leq 1$

$$\theta = (\theta_8(4(1-x)) + \theta_9(4(x-\frac{y}{c})) + \theta_{10}(\frac{4y}{c}-3)) H(1-\tau_6) \quad (\frac{2}{3} \leq x \leq 1)$$

The dimensionless Nusselt numbers (Nu) and Sherwood Numbers (Sh) on the non-insulated boundary walls of the rectangular duct are calculated using the formula

$$Nu = \left( \frac{\partial \theta}{\partial x} \right)_{x=}$$

Nusselt Number on the side wall  $x=1$  in different regions are

$$Nu_1 = 2 - 4\theta_3 \quad (0 \leq y \leq h/3)$$

$$Nu_2 = 2 - 4\theta_6 \quad (h/3 \leq y \leq 2h/3)$$

$$Nu_3 = 2 - 4\theta_8 \quad (2h/3 \leq y \leq h)$$

## **DISCUSSION OF THE NUMERICAL RESULTS**

In this analysis we investigate the effect of chemical reaction on the mixed convective heat transfer flow of a viscous electrically conducting fluid through a porous medium in a rectangular cavity.

The non-dimensional temperature ( $\theta$ ) is shown in figs 1-4 at different horizontal and vertical levels with variations in Ra,  $N_1$ ,  $\alpha$  and Ec. The variation of non dimensional temperature ( $\theta$ ) with Rayleigh number Ra at horizontal and vertical levels, it is found that the actual temperature enhances with  $Ra \leq 2 \times 10^2$  and depreciates with higher  $Ra \geq 3 \times 10^2$  also it

reduces with  $|Ra|$  at all horizontal levels (fig 1 and 2). At the higher vertical level  $x = \frac{2}{3}$ , it enhances with  $Ra \leq 2 \times 10^2$  and depreciates  $Ra \geq 3 \times 10^2$ . Also it reduces with  $|Ra|$  at  $x = \frac{1}{3}$  and  $x = \frac{2}{3}$  levels (figs. 3 and 4). It is found that the temperature at the horizontal levels is greater than that at the vertical levels. The variation of non-dimensional temperature ( $\theta$ ) with radiation parameter  $N_1$  is shown in fig 5-8 at different levels, it is found that higher the radiative heat flux larger the actual temperature at  $y = \frac{2c}{3}$  level and smaller at  $y = \frac{c}{3}$  level. Whole at the vertical it depreciates with  $N_1$  (fig 7&8).

Fig 9-12 represent non dimensional temperature ( $\theta$ ) with heat source parameter  $\alpha$  it is found that the actual temperature experiences depreciation at all horizontal and vertical levels with increase in the strength of the heat source while the increase in the strength of the heat sink enhances the actual temperature at all the levels. It is found that the temperature at the vertical levels is greater than that at the horizontal source. The variation of non-dimensional temperature ( $\theta$ ) with Eckert number  $E_c$  is shown in fig 13-16 at horizontal and vertical levels. it is found that the higher the dissipative heat smaller the actual temperature at all the levels fig(13-16). It is noticed that the variation of  $\theta$  at the vertical levels is greater than that at the horizontal levels.

The rate of heat transfer for different values  $Ra$ ,  $N_1$ ,  $\alpha$  and  $E_c$  is shown in table 1-4. The variation of  $N_u$  with Rayleigh number  $Ra$  at different level shows that the  $N_u$  at the lower and upper quadrant enhances with increase in  $Ra$  while in the middle quadrant it depreciates with  $Ra$  (Table-1). Table-2 shows that the variation of  $N_u$  with radiation parameter  $N_1$ . It is shown that the rate heat transfer at the lower and middle quadrant enhances with  $N_1 \leq 0.07$  and reduces with  $N_1 \geq 0.09$  whole at the upper quadrant it reduces with  $N_1$ .

The variation of  $N_u$  with heat source parameter  $\alpha$  is shows in Table-3. In entire region it is found that the rate of heat transfer enhances with increase in the strength of the heat source and depreciates with that of heat sink at all quadrants. The variation of  $N_u$  with Eckert number  $E_c$  shows in the Table-4 that higher the dissipative heat larger  $|N_u|$  at all quadrant.

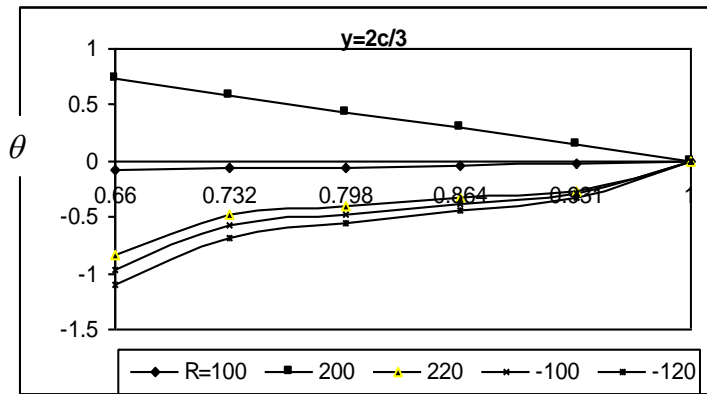


Fig. 1 Variation of  $\theta$  with Ra at  $y = 2c/3$  level  
 $Ec = 0.001, \alpha = 2, N_1 = 0.01$

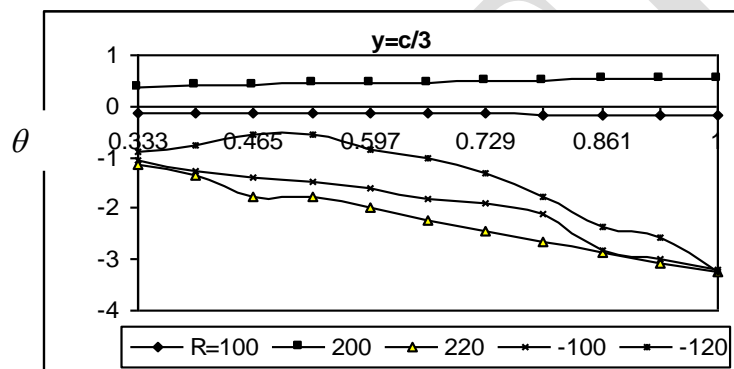


Fig. 2 variation of  $\theta$  with Ra at  $y = c/3$  level  
 $Ec = 0.001, \alpha = 2, N_1 = 0.01$

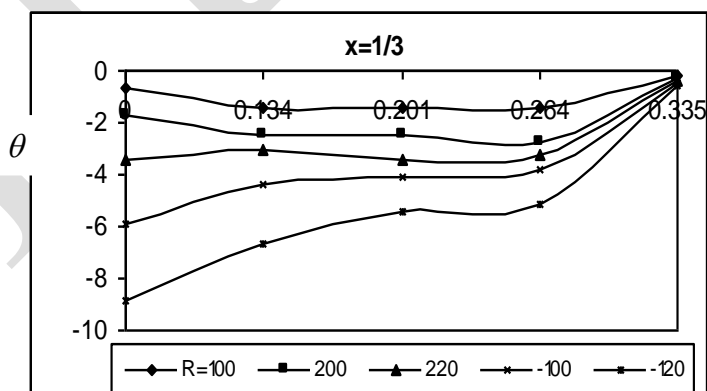


Fig. 3 variation of  $\theta$  with Ra at  $x = 1/3$  level  
 $Ec = 0.01, \alpha = 2, N_1 = 0.01$

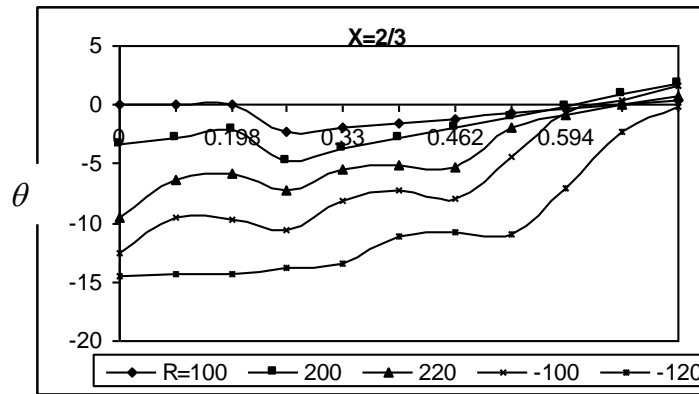


Fig. 4 variation of  $\theta$  with Ra at  $x = 2/3$  level  
 $Ec = 0.01, \alpha = 2, N_1 = 0.01$

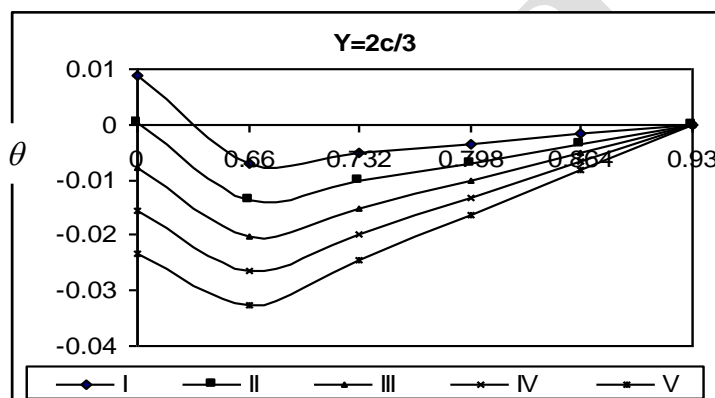


Fig. 5 variation of  $\theta$  with  $N_1$  at  $y = 2c/3$  level  
 $Ra = 100, Ec = 0.001, \alpha = 2$

	I	II	III	IV	V
$N_1$	0.01	0.03	0.05	0.07	0.09

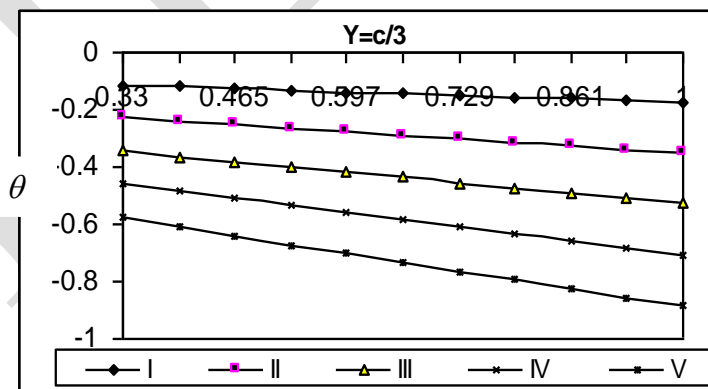


Fig. 6 variation of  $\theta$  with  $N_1$  at  $y = c/3$  level  
 $Ec = 0.001, Ra = 100, \alpha = 2$

	I	II	III	IV	V
$N_1$	0.01	0.03	0.05	0.07	0.09

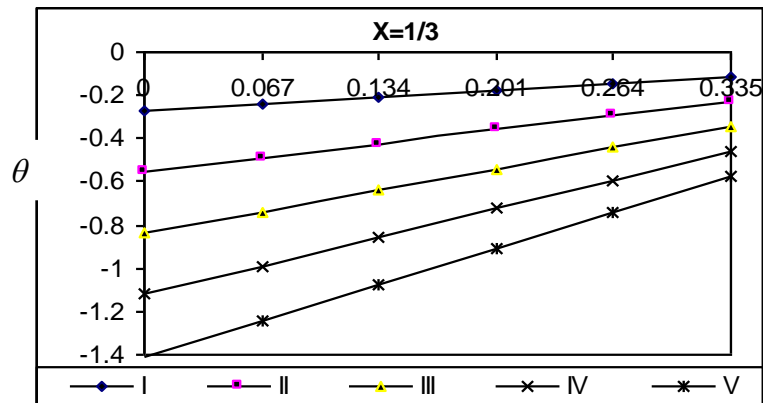


Fig. 7  $\theta$  variation with  $N_1$  at  $x = 1/3$  level

$Ec=0.001, Ra = 100, \alpha=2$

	I	II	III	IV	V
$N_1$	0.01	0.03	0.05	0.07	0.09

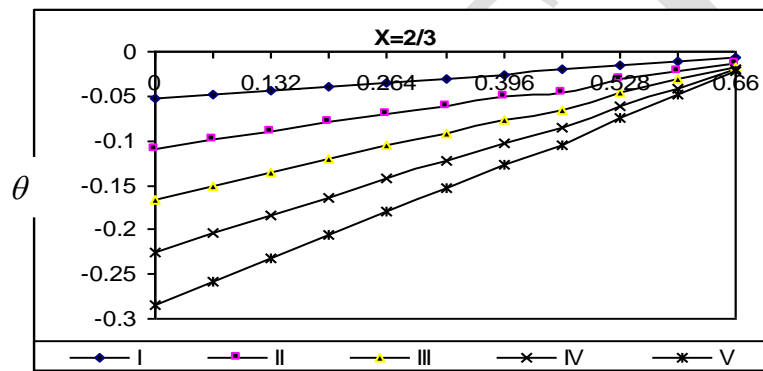


Fig. 8 variation of  $\theta$  with  $N_1$  at  $x = 2/3$  level

$Ec=0.001, Ra = 100, \alpha=2$

	I	II	III	IV	V
$N_1$	0.01	0.03	0.05	0.07	0.09

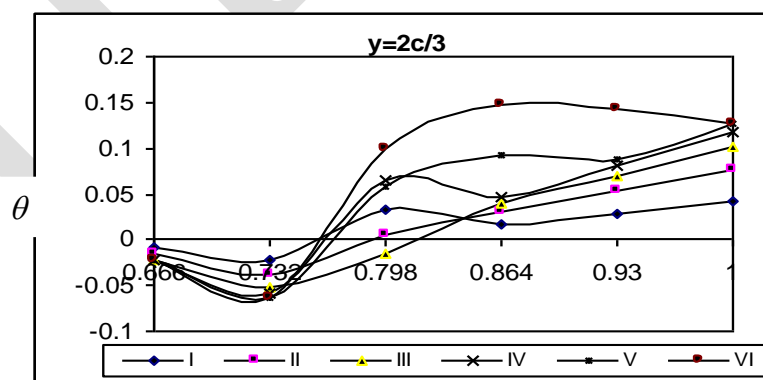


Fig. 9 variation of  $\theta$  with  $\alpha$  at  $y = 2c/3$  level

$Ra = 100, Ec=0.001, N_1=0.01$

	I	II	III	IV	V	VI
$\alpha$	2	4	6	-2	-4	-6

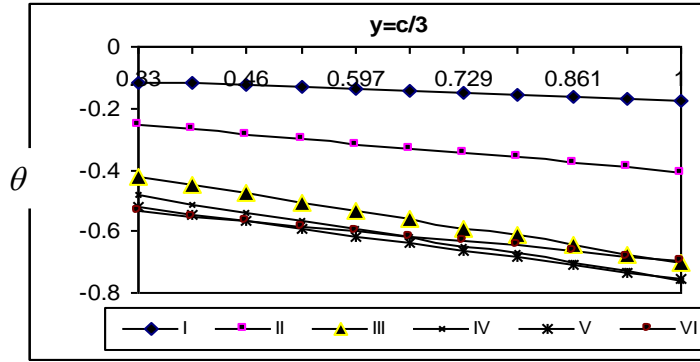


Fig. 10 variation of  $\theta$  with at  $\alpha y = c/3$  level

$Ra = 100, Ec=0.001, N_1 = 0.01$

	I	II	III	IV	V	VI
$\alpha$	2	4	6	-2	-4	-6

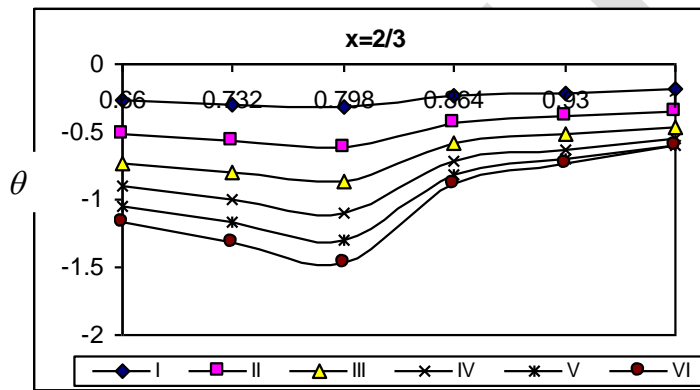


Fig. 11 variation of  $\theta$  with at  $\alpha x = 2/3$  level

$Ra = 100, Ec=0.001, N_1 = 0.01$

	I	II	III	IV	V	VI
$\alpha$	2	4	6	-2	-4	-6

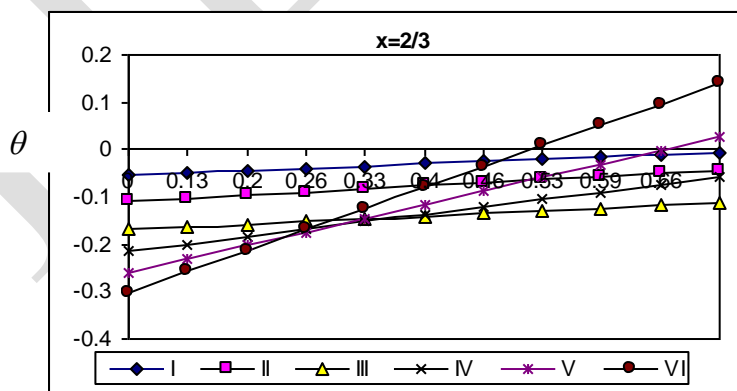


Fig. 12 variation of  $\theta$  with  $\alpha$  at  $x=2/3$  level

$Ra = 100, Ec=0.001, N_1 = 0.01$

	I	II	III	IV	V	VI
$\alpha$	2	4	6	-2	-4	-6



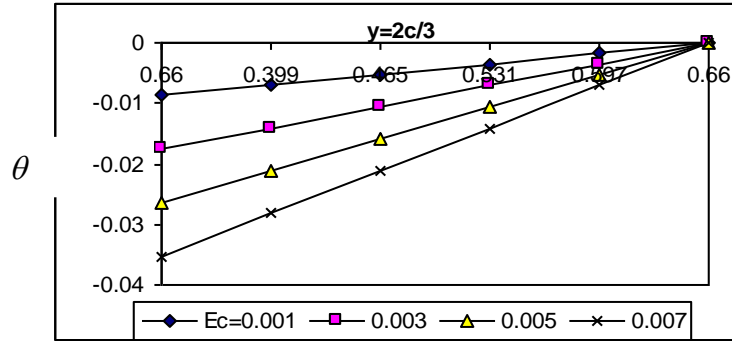


Fig. 13 variation of  $\theta$  with  $Ec$  at  $y=2c/3$  level  
 $Ra = 100, \alpha=2, N_1=0.01$

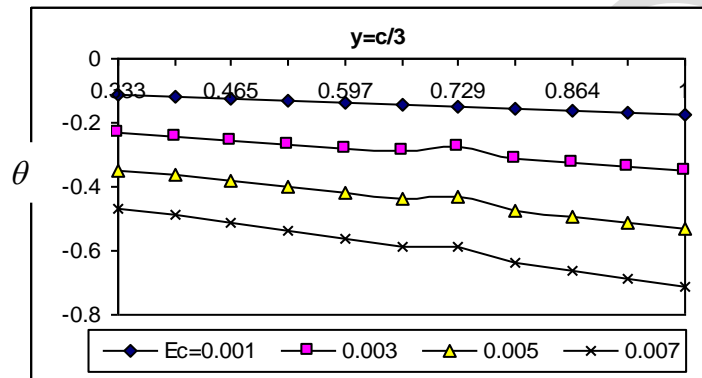


Fig. 14 variation of  $\theta$  with  $Ec$  at  $y=c/3$  level  
 $Ra = 100, \alpha=2, N_1=0.01$

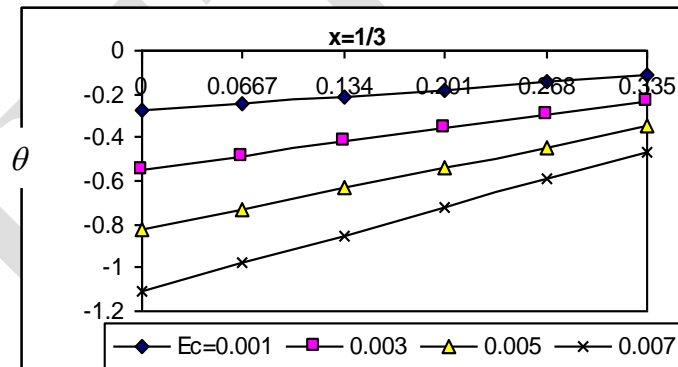


Fig. 15 variation of  $\theta$  with  $Ec$  at  $x=1/3$  level  
 $Ra = 100, \alpha=2, N_1=0.01$

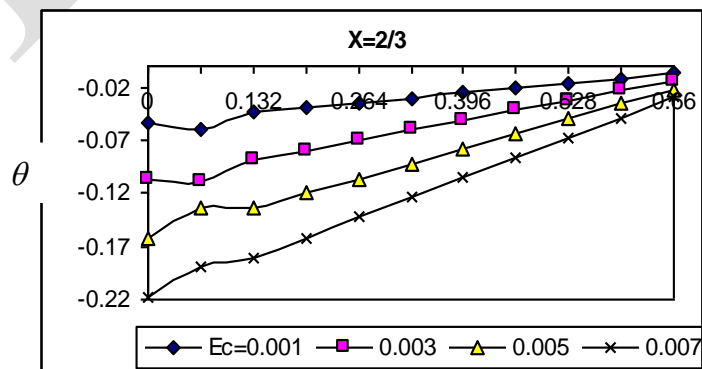


Fig. 16 variation of  $\theta$  with  $Ec$  at  $x=2/3$  level  
 $Ra = 100, \alpha=2, N_1=0.01$

Table-1  
 Nusselt Number (Nu) at different levels

Nu <sub>1</sub>	2.06412	1.528	4.756	1.2352	1.582
Nu <sub>2</sub>	8.1628	7.188	6.43524	4.7528	4.3602
Nu <sub>3</sub>	5.036	-3.4624	5.92	-1.0643	-1.4126
Ra	1x10 <sup>2</sup>	2x10 <sup>2</sup>	3x10 <sup>2</sup>	-1x10 <sup>2</sup>	-2x10 <sup>2</sup>

Table-2  
 Nusselt Number (Nu) at different levels

Nu <sub>1</sub>	2.2128	2.237	2.268	2.364	2.0323
Nu <sub>2</sub>	2.1198	2.1296	2.142	2.258	2.175
Nu <sub>3</sub>	2.0269	2.0224	2.018	2.0136	2.0096
N <sub>1</sub>	0.01	0.03	0.05	0.07	0.09

Table-3  
 Nusselt Number (Nu) at different levels

Nu <sub>1</sub>	2.2128	2.2248	2.2368	2.1891	2.1778	2.16692
Nu <sub>2</sub>	2.11988	2.1870	2.2544	2.0135	1.9202	1.8546
Nu <sub>3</sub>	2.0269	2.1493	2.2720	2.2163	1.6627	1.54244
α	2	4	6	-2	-4	-6

Table-4  
 Nusselt Number (Nu) at different levels

Nu <sub>1</sub>	2.2128	2.2242	2.2356	2.2431
Nu <sub>2</sub>	2.11988	2.13052	2.1592	2.1818
Nu <sub>3</sub>	2.0268	2.0408	2.0706	2.0808
E <sub>c</sub>	0.001	0.003	0.005	0.007

## REFERENCES

1. Badruddin, I. A, Zainal, Z.A, Aswatha Narayana, Seetharamu, K.N: "Heat transfer in porous cavity under the influence of radiation and viscous dissipation," *Int. Comm. In Heat & Mass Transfer* 33 (2006), pp, 491-499.
2. Brinkmann, H.C: A calculation of the viscous force external by a flowing fluid on a dense swarm of particles: *Applied science Research*, Ala, p 81, (1948).
3. Cheng K.S. and J.R. Hi., : Steady, Two-dimensional, natural convection in rectangular enclosures with differently heated walls *transaction of the ASME*, v. 109, p, 400, (1987).
4. Cheng P : heat Transfer in Geo-thermal system, "Advances in Heat Transfer", V.14, pp. 1-105 (1979).
5. Chien-Chang Huang, Wie-Mon Yan, Jer-Huan Jang: Laminar mixed convection heat and mass transfer in vertical rectangular ducts with film Evaporation and condensation, *Int. J. of Heat and Mass Transfer* Vol. 48, pp 1772-1784 (2005).
6. Combarous and Bories : *J. Fluid Mech.*, pp 63-93 (1973)
7. Combarous M : "National Convection in Porous media and Geo-thermal systems", 6<sup>th</sup> *Int. Heat Transfer conf*; Totonto, p. 45-59 (1978).
8. Foroboschi F P and Federico T P : *Int. J. Heat Mass Transfer*, v-7, p. 315 (1964)
9. Kilic M : Determinations of heat transfer rate and Nusselt number on the thermal-entry region in ducts, *Int. Comm. Heat Mass Transfer*, Vol. 31, No. 2, pp. 181-190 (2004).
10. Nagaradhika V: Mixed convective heat transfer through a porous medium in a Corrugated channel/ducts, Ph.D. thesis, S.K. University (2010)
11. Padmavathi, A: Finite element analysis of the Convective heat transfer flow of a viscous in compressible fluid in a Rectangular duct with radiation, viscous dissipation with constant heat source, *Jour. Phys and Appl.Phys.*,V.2 (2009).
12. Prasad, V. and Kulacki, F.A : Convective heat transfer in a rectangular porous cavity effect of aspect ratio flow structure and heat transfer, *ASME Journal of heat transfer* v. 106, pp, 158-165 (1984).
13. Prasad, V. and Kulacki, F.A : Natural convection in a vertical porous annulus, *Int. J. Heat mass transfer*, v. 27, pp, 207-219 (1984).
14. Rangareddy, M: Heat and Mass transfer by Natural convection through a porous medium in ducts ,Ph. D thesis, S.K. University, Anantapur(1997)
15. Sivaiah, S: Thermo-Diffusion effects on convective heat and mass transfer through a porous medium in Ducts, Ph.D thesis, S.KUniversity, Anantapur, India (2004).
16. Sreenivas G: Finite Element Analysis of convective flow and heat transfer through a porous medium with dissipative effects in channels/ Ducts, Ph. D. Thesis , S. K. University (2005)
17. Verschoor, J.D, and Greebler, P : Heat Transfer by gas conduction and radiation in fibrous insulation *Trans. Am. Soc. Mech. Engrs.* PP, 961-968 (1952).